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# Characterization of Polyaniline and Poly (*m*-toluidine)-based Nanoparticles of Ultranarrow Particle Size Distribution

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The oxidative polymerization of aniline or m-toluidine, carried out in concentrated solutions of poly(vinyl alcohol-co-acetate)  $(PVA)$ , was used to prepare colloidal composite particles of polyaniline-PVA or poly(m-tohidine)-PVA of ultranarrow particle size distribution and of controlled average particle size. The particle size distributions were measured by quasi-elastic light scattering in diluted polymerization products. Such a measurement can be influenced by undestroyed PVA aggregates formed in the initial solution. The aim of this work was to determine conditions under which the **true** particle size distribution of the composite particles can be measured or, at least, estimate the degree such a determination is intluenced by PVA aggregates not incorporated into the composite particles. Quasi-elastic light scattering measurements of the diluted polymerization products were carried out under various experimental conditions. The composite particles were separated from the PVA solution by centrifugation and redispersed in water. The size of the redispersed composite particles and *of* the PVA aggregates in the supernatant solution was measured again by quasi-elastic light scattering. Scanning electron microscopy showed the spherical shape of the synthesized composite particles and confirmed their ultranarrow size distribution.

 $Keywords:$  Colloidal particles; Poly(aniline or *m*-toluidine)-poly(vinyl alcohol-coacetate) composite particles; Quasi-elastic light scattering; Viscometry; Centrifugation; Scanning electron microscopy

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## **INTRODUCTION**

Studies of the oxidative polymerization of the aniline and  $m$ -toluidine have shown higher reactivity of  $m$ -toluidine,  $[1,2]$  concerning the addition of the monomer to the growing chains. Consequently, the polymerization of  $m$ -toluidine proceeds at a lower concentration of active sites in comparison with aniline. The increase of temperature also facilitates monomer addition to the oxidized dimer with the same consequence, *i.e.*, lowering the concentration of the growing chains. As a result, it has been proposed  $[3]$  that a monomer of adequate reactivity (aniline or  $m$ -toluidine) with an appropriate steric stabilizer, such as the poly(viny1 alcohol-co-acetate) (PVA), and a suitable choice of monomer and oxidant concentrations could be used to manipulate the growth rate of the colloidal particles. This idea was verified<sup>[3]</sup> by preparing tailor-made suspensions of the colloidal composite particles of polyaniline-PVA and  $poly(m\text{-}toliidine)$ -PVA (PMTD-PVA) of ultranarrow particle size distribution **(PSD)** and a controlled average particle size within the range of **<sup>200</sup>**- **<sup>3000</sup>**nm. The polymerizations were carried out in concentrated PVA solutions.

The average particle size and the PSD of the polyfaniline or *m*tohidine)-PVA composite particles were obtained from quasi-elastic light scattering **(QELS)** measurements **[31** of diluted polymerization products. Unfortunately, the results of the **QELS** measurements can be influenced by the PVA aggregates. As a matter of fact, the initial PVA solutions before the polymerization contain large PVA aggregates whose average size is of the order of  $1 \mu m$  and it was not known whether or not these aggregates are destroyed during the polymerization of the aniline or  $m$ -toluidine. Consequently, our previous study<sup>[3]</sup> is extended here in order to confirm our conclusions concerning the average size and the size uniformity of the tailor-made composite particles.

The principal objectives of this study were to determine: the amount of the PVA remaining free in solution after polymerization of aniline or  $m$ -toluidine relative to the PVA that is incorporated in the synthesized composite particles; the size of the PVA aggregates in the supernatant solution of the centrifuged suspension after polymerization, as well as in the centrifuged initial PVA solutions before polymerization; and the true size and shape of the composite particles.

## **EXPERIMENTAL**

#### **Polymerization**

Reagent-grade aniline and  $m$ -toluidine, as well as all other reagents, were purchased from Fluka (Germany). The suspensions of poly(aniline) (PAN1)-PVA and PMTD-PVA were prepared by oxidative polymerization of monomers using PVA as a steric stabilizer (degree of polymerization 1600, degree of hydrolysis  $86\%$  w/w), and ammonium peroxydisulphate as oxidant in the presence of formic acid.

The course of the polymerization of  $m$ -toluidine was studied by taking small quantities of samples from the reaction mixture at different times and by measuring the average particle size and PSD by QELS and the relative viscosity of the diluted reaction mixture. Polymerization in these samples was stopped immediately after sampling by the addition of NaOH solution to obtain pH value of **9-** 10. Preliminary measurements of the average particle size and PSD of a PANI-PVA sample suspended in aqueous acid or alkaline solutions at different pH values showed negligible influence of the pH value of the medium on the particle size and PSD of the suspensions.

## **Quasi-elastic Light Scattering**

Model Zetamaster, Malvern Instruments, Ltd., Malvern, Worcestershire (U. K.) was used to measure the average particle size and PSD of the PVA aggregates in solution and of the polymerized samples.

The QELS measurements were made on i. the initial PVA solutions of different concentrations without and with the addition of the polymerization reaction components, of the resulting suspensions after the polymerization of the aniline or  $m$ -toluidine, ii. the supernatant PVA solution after the elimination of the composite particles by centrifugation, and iii. the redispersed composite particles in water. These measurements were made to estimate the degree in which determination of the **PSD** of the composite particles is influenced by free **PVA** remaining in solution and form aggregates, and whether or not **PVA** aggregates are destroyed or their size modified during polymerization.

### **Vlscometty**

**A** standard Ubbelohde capillary viscometer with **AVS** 410 model, Schott, (Germany) automatic viscometer was used to measure the relative viscosities (relative to water) of all PVA solutions and of the polymerization products. The measurements were performed at **25°C.** 

The viscometry was used to determine the concentration of the **PVA** in the supernatant solution after polymerization of aniline or m-toluidine and after the separation of the composite particles by centrifugation. The amount of PVA incorporated into the composite particles **can** be calculated from the viscometry data. Since the viscosity of the **PVA** supernatant solutions can be influenced **by** the components of the polymerization reaction, the relative viscosities of the **PVA** solutions of different concentrations were measured without and with the addition of the reaction components (aniline or m-toluidine and formic acid, but not the oxidant which starts the polymerization).

#### **Centrifugation**

Model 4239 R, **ALC,** Milan (Italy) high-speed refrigerated centrifuge equipped with a swinging-bucket rotor was used to separate the composite particles from the supernatant **PVA** solution. **A** rotation speed of **6000rpm,** corresponding to the acceleration of *6500G,* was chosen with respect to the time of centrifugation. All centrifugations were carried out at 25°C.

## **Scannlng Electron Mlcroscopy**

Model Jeol 7410 **LV,** (Japan) **scanning** electron microscope was used to visualize the form of the synthesized composite particles and to check their **size** and size distribution under dry conditions where the thickness of the adsorbed **PVA** chains forming the shell of the particles was minimized.

## **RESULTS AND DISCUSSION**

## **Effect of the Components of Polymerization Reaction of Aniline on the Relative Viscosity of PVA Solutions and on the Size of PVA Aggregates**

The relative viscosities of the **PVA** solutions as a function of the concentration without and with the addition of the same amount of aniline and formic acid as for the polymerization is shown in Figure 1. It can be seen that the addition of the polymerization reaction components results in a small increase of the relative viscosity of **PVA**  solutions. This can be due to the modified swelling of the polymer chains or due to the displacement **of** the equilibrium between the free polymer chains and **PVA** aggregates in solution.



**FIGURE 1 Relative viscosities of PVA solutions at different concentrations without and with the addition of the components of the aniline polymerization and with the addition of NaC1. The experimental data concerning the PVA solutions with NaCl are**  taken from Ref. [4].

The results of the **QELS** measurements of the particle size of the **PVA** aggregates shown in Figure **2** are strongly concentration dependent. The increase of the size of the **PVA** aggregates is most pronounced above a concentration of  $2\%$  (w/w) of the PVA. However, it must be taken into account that the autocorrelation function used to treat the **QELS** measurements provides the diffusion coefficient values and the corresponding particle sizes are, in fact, calculated from

$$
d = \frac{kT}{3\pi\eta D} \tag{1}
$$

where *d* is the particle diameter, *k* is the Boltzmann constant, *T* is the temperature,  $\eta$  is the viscosity of the suspending liquid, and *D* is the diffusion coefficient. The value of the viscosity of the suspending liquid (water in this case) must be introduced as one of the **QELS** software input data for the calculation of the **PSD.** The problem is that some of the measurements were performed in relatively concentrated **PVA**  solutions whose bulk viscosities were much higher than the viscosity of pure water. Consequently, the effective diffusion coefficients of the



**FIGURE 2 Average particle size of the PVA aggregates as a function of the PVA concentration in solutions without and** with **the addition of components of the aniline polymerization.** 

PVA aggregates should be lower in the concentrated PVA solutions which should result in higher apparent sizes of the measured aggregates. The substitution of the viscosity of pure water by the bulk viscosity of the PVA solution in the calculations should compensate this error, but the bulk viscosity of the solution includes the contribution of the PVA aggregates whose exact equilibrium concentration is difficult to determine. The input of the bulk viscosity of PVA solution instead of the viscosity of water substantially modified the resulting values of the particle size for the PVA solutions of the highest concentrations, as can be seen in Table I. The conclusion from these measurements is that the concentration of the PVA solutions should be below 2% (w/w) in order to obtain reliable **QELS**  results, independent of the introduced solvent viscosity.

Although the polymerization reaction components have an irregular effect on the **QELS** measurement of the particle size of PVA aggregates at higher PVA concentrations, the size of the PVA aggregates is systematically lower for the diluted solutions containing the polymerization components (roughly **50%** of the average size values obtained for the PVA solutions of the same concentrations but without the polymerization components), as can be seen in Figure **3,** which is an enlarged area of the low concentration range in Figure 2.

Investigation of the effect of NaCl on the behavior of PVA solutions indicated that although the relative viscosities were not substantially modified by NaCl (see experimental data in Fig. 1) in comparison with the solutions of the same concentration of the PVA but without the addition of NaC1, the measurement of the PSD by **QELS** proved the progressive destruction of PVA aggregates with increasing NaCl concentration. **[41** These results, see Figure **4,** show the variation of the

Concentration of PVA solution $(\frac{6}{w})w$	Calculated size (nm) using viscosity of <b>PVA</b> solution	Calculated size (nm) using viscosity of water
8	220	46 196
4	1493	14 100
$\overline{2}$	1416	2035

**TABLE I Effect of input viscosity** on the **average particle size calculated** from **QELS measurement of PVA solutions** 



**FIGURE 3 Average particle size** of **the PVA aggregates and of the synthesized PANI-PVA composite particles as a function** of **the PVA concentration in solutions without and with the addition** of **the components** of **the aniline polymerization.** 



**FIGURE 4 Average particle size** of **the PVA aggregates as a function** of **NaCl concentration in the PVA solution at a concentration** of **1** % **(w/w).** 

**average size of the PVA aggregates with NaCl concentration in 1** % **(w/ w) PVA solutions. It seems reasonable to explain these results** of **the QELS measurements** by **a partial destruction** of **the PVA aggregates.** 

## **Sedimentation of PVA Aggregates During Centrifugation**

In order to elucidate whether the concentration of the **PVA** in solution varies due to sedimentation of **PVA** aggregates during centrifugation, two **PVA** solutions **(30** ml each) at **4%** w/w without and with the aniline polymerization components were centrifuged during 121 h at 6000 rpm and measured subsequently by QELS and viscometry. **A** volume of 0.5ml of each solution was taken near the meniscus for **QELS** measurement. The average particle size was 157 nm for the **PVA** solution without polymerization components and 36nm with components. These results indicate that the largest **PVA** aggregates can sediment under the conditions of centrifugation because the measured average particle sizes were at least **3** to 10 times lower than the lowest values (see Fig. **2)** obtained for the same solutions before centrifugation. Moreover, a small polymer cake was observed at the bottom of the sedimentation tubes after centrifugation. However, the relative viscosities of the initial **PVA** solutions before centrifugation and of upper fractions (representing *85%* of the solution) after the centrifugation were practically identical (see Tab. **11)** for the **PVA** solutions with and without the addition of the polymerization components. It indicates that the sedimenting **PVA**  aggregates probably do not significantly influence the viscosity of the **PVA** solution to their relatively low concentration. More detailed investigation of the sedimentation of the **PVA** aggregates was not required.

**TABLE I1 Relative viscosities of PVA solutions without and with the polymerization reaction components before centrifugation and of upper fractions after the centrifugation** 

	Relative viscosity before centrifugation	Relative viscosity of upper fraction after centrifugation
PVA solution without polymerization components	11.24	11.89
PVA solution with polymerization components	11.68	11.98

## **Size of PANI-PVA Composite Particles Measured by QELS in Diluted Polymerization Products**

Three polymerizations of aniline were carried out in **PVA** solutions. The **PSD** and the average particle size of the diluted suspensions after polymerizations were determined by the QELS. **A** typical result is in Figure **3** showing the average particle size measured for one suspension at different concentrations and in Figure 5 which shows the **PSD** of the **PVA** aggregates in the initial **PVA** solution and the **PSD** of one of the diluted polymerization products. The results demonstrated in Figure 5 represent excellent reproducibility of the polymerization of the aniline under the given conditions because almost the same **PSD** values were obtained previously. **[31** However, with regard to the experimental findings demonstrated, especially in Figure **3,** the attribution of the definite **PSD** to the composite **PANI-PVA** particles was questionable because almost the same **PSD**  values were obtained for the **PVA** aggregates in solutions with the addition of the polymerization components. The results of a more detailed investigation of this point are discussed in the following paragraphs.



**FIGURE 5 Particle size distributions of** i. **PVA aggregates in solution before polymerization, ii. of the composite PAM-PVA particles in diluted polymerization product, and of iii. the PANI-PVA particles after their separation from excess PVA solution by centrifugation and redispersion of the sediment** in **water.** 

## **Relative Viscosity of the Suspension After Polymerization and of the Supernatant Solution After Centrifugation**

The relative viscosity of the diluted **(4%** wjw of **PVA)** suspension of the composite particles **PANI-PVA** after polymerization of the aniline was  $\eta = 15.92$ , which is higher (by about  $36\%$ ) as compared with the relative viscosity  $\eta = 11.68$  of the PVA solution with the polymerization reaction components (see Fig. 1) before polymerization. The synthesized composite particles were separated from the **PVA** solution by centrifugation of 20mL of suspension. The relative viscosity of the upper fraction of the colorless supernatant **PVA** solution (after centrifugation) was  $\eta = 12.58$  thus comparable with the relative viscosity  $\eta = 11.68$  of the initial PVA solution. The volume of the lower fraction was not sufficient to measure the relative viscosity without dilution. The relative viscosities of higher  $(\eta = 3.01)$  and lower  $(n = 2.99)$  fractions diluted to 2% (w/w) of PVA were identical within the range of experimental errors and only slightly higher than the relative viscosity of the initial solution  $\eta = 2.93$  (with the polymerization reaction components) at the same concentration (see Fig. 1). The relative viscosity of the whole suspension diluted to  $2\%$  (w/w) of PVA was  $\eta = 3.25$ . The sedimented **PANI-PVA** particles were redispersed in 20mL of water. The relative viscosity of this redispersed suspension was  $\eta = 1.03$ .

The above relative viscosities imply that only a small part of the **PVA** is incorporated in the separated and redispersed **PANI-PVA**  particles. The concentration and, consequently, the relative viscosity of the **PVA** remaining in supernatant solution **is** only moderately changed by the polymerization of aniline. All viscosity data indicate that the composite **PAM-PVA** particles behave practically as **sus**pended hard spheres.

## **Size of the Composite PANI-PVA Particles After Separation by Centrifugation and Redispersion in Water**

The size of the composite **PANI-PVA** particles redispersed **in** water after their separation from the **PVA** supernatant solution by centrifugation was measured by **QELS** and its constant average value of 220 nm was practically independent on the concentration of the suspension. The standard deviation of the **PSD** was **86** nm. The entire **PSD** of the **PAN1** particles separated from the excess **PVA** solution by centrifugation, repeatedly redispersed and centrifuged in water is shown in Figure 5. The width of the PSD of these particles is almost the same as that measured directly by **QELS** in diluted suspension after the polymerization; however, the entire **PSD** and, of course, the average particle size are shifted to lower values, probably due to the reduced contents of the undestroyed **PVA** aggregates. The average particle size and the standard deviation of the **PSD** of this sample measured by **QELS** before the elimination of the **PVA** solution by centrifugation were **370** nm and **13** 1 nm, respectively. The **QELS**  measurement was performed within the range of **PVA** concentrations assured to be low enough to suppress the above mentioned concentration effects.

### **Scanning Electron Microscopy**

The image from the scanning electron microscopy **(SEM)** of the **PAM-PVA** particles is shown in Figure **6.** It demonstrates that the particles are almost perfectly spherical and their **PSD** is ultranarrow



**FIGURE 6 Scanning electron microscopy photography of PANI-PVA composite particles.** 

thus confirming the QELS measurements. Obviously, the average particle size seen on the **SEM** image is lower in comparison with the QELS measurements because of the substantially reduced thickness of the PVA shell due to the drying of the deposited sample.<sup>[4]</sup> As the number of the particles in Figure *6* is relatively low, the calculation of the PSD from the **SEM** image was not done.

## **Polymerization of mtoluidine**

Relatively slow polymerization of *m*-toluidine allows samples to be taken from the polymerization mixture for following the relative viscosity of the intermediate polymerization product, as well **as** the evolution of the **PSD,** starting from the PVA aggregates up to the composite particles formed during polymerization. The evolution of the **PSD** shown in Figure **7** confirmed, in this case too, good reproducibility of  $m$ -toluidine polymerization. Practically the same result was obtained previously.<sup>[3]</sup>

Small volume samples of 2mL each were taken each hour from the polymerizing suspension (whose initial volume was **30 mL)** and diluted 10 times with 0.25 **M** NaOH which immediately stops the polymerization. The relative viscosities of the diluted samples were measured to



FIGURE **7** Evolution of the particle size distribution of samples taken from the reaction mixture at different stages of the polymerization of m-toluidine, starting from the initial PVA solution until the end of the polymerization, and particle size distribution of the poly(m-tohidine)-PVA particles after their separation from excess PVA solution by centrifugation and redispersion of the sediment in water.

follow polymerization with time. Thereafter, the diluted samples were centrifuged during **23** h and the relative viscosities of the upper and lower half of the samples diluted 2.5 times further were measured again. The results are shown in Figure **8.** It can be concluded that the relative viscosity of the samples does not change significantly during polymerization of  $m$ -toluidine. Centrifugation does not have significant effect on the distribution of the free PVA in the supernatant solution because no important difference in the relative viscosities between the higher and lower diluted fractions could be detected.

The **QELS** measurements of the upper and lower fractions after centrifugation provided a series of average particle sizes fluctuating with polymerization time the samples were taken. These results can be seen in Figure 9 which shows, for the sake of comparison, also the average particle sizes measured directly in raw diluted suspensions before the elimination of excess of PVA by centrifugation.

The sediments of  $poly(m\text{-}toliidine)-PVA$  (PMTD-PVA) particles obtained by centrifugation of the samples taken at different polymerization times were redispersed in water and their PSD values measured by **QELS** at different concentrations. The mean value of nation of excess of PVA by centrifugation.<br>
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FIGURE 8 Variation of the relative viscosity during the polymerization of *m*-toluidine **measured** in **the raw diluted polymerization product and** in **upper and lower fractions taken from the sedimentation tubes after centrifugation and additional dilution.** 



**FIGURE 9 Variation of the average particle size during the polymerization of** *m***toluidine measured in the raw diluted polymerization product and in upper and lower fractions taken from the sedimentation tubes after centrifugation and additional dilution.** 

eleven independent measurements gave an average particle size of 360 nm with a standard deviation of 66 nm. No other than statistical fluctuations of the average particle size has been observed from sample to sample with no systematic correlation as a function of the polymerization time or of the concentration of the particles. **A** typical **PSD** of the redispersed **PMTD-PVA** particles is shown in Figure **7.** 

Similarly as in the case of the **PANI-PVA** particles, the width of the **PSD** of the **PMTD-PVA** washed and redispersed particles is almost the same as that measured by QELS directly in diluted **PMTD-PVA**  suspension at the end of the polymerization. Nevertheless, the average particle size of the redispersed **PMTD-PVA** sample is 351nm, the standard deviation of the **PSD** is 109nm, which is shifted, again, to a lower value as well as the entire PSD as compared with the average particle size of 470nm and the standard deviation of the **PSD** of 165nm of the same sample before centrifugation, washing and redispersion. These differences can probably be due to the reduced contents of the undestroyed **PVA** aggregates in the redispersed sample as well as to the reduced effective size of the washed and redispersed **PMTD-PVA** particles.

## **CONCLUSION**

It has been found that particles of uniform size are formed within a limited period of time during the polymerization, in some cases until termination. Their sizes lie within the range from 200 to 600nm for PANI and from 400 to 3000 nm for poly(*m*-toluidine). The PANIbased colloidal particles synthesized in this work exhibit at least the same but in most cases a narrower PSD as compared with commercially available uniform PS latex standards. Such a comparison was already demonstrated.<sup>[3]</sup> The determination of the PSD and of the average particle size of the composite PANI-PVA and PMTD-PVA colloidal particles by the **QELS** is a delicate task. However, accurate values can be obtained provided that conditions of measurement are established in such a manner as to avoid artifacts due to the particular behavior of PVA solutions.

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